



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane
 Bill of Lading date 07-Oct-14

ChevronTexaco

CONTENTS LISTING

We have pleasure in enclosing herewith, our report for the above referenced inspection.
 The inspection was carried out according to the following reports:

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Should you have any query, or require any additional information, please contact Mr. Chris Sherfield at our Houston office (telephone number +1 281 488 7673).

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane

SUMMARY OF QUANTITIES
 Page 1 of 2
 Comparison of Ship's figures and Bill of Lading

			Bill of Lading figures:		
BOL No.	Product name	BOL date	US Barrels at 60°F	US Gallons at 60°F	Pounds in air
1	Butane	07-Oct-14	8,956.03	376,153.26	1,827,916.77
2	LPG mix	07-Oct-14	13,790.55	579,203.10	2,591,122.99

BOL No.	Long Tons	Short Tons	Metric Tons in air	Metric Tons in vacuo	Pounds in vacuo
1	816.034	913.958	829.130	830.717	1,831,414.99
2	1,156.751	1,295.561	1175.315	1177.758	2,596,509.58

Total Bill of Lading Quantities

Totals of the Bills Of Lading	LPG mix	Butane		Total
US Barrels at 60°F :	13,790.55	8,956.03		22,746.58
US Gallons at 60°F :	579,203.10	376,153.26		955,356.36
Pounds in air:	2,591,122.99	1,827,916.77		4,419,039.76
Long Tons :	1,156.751	816.034		1,972.785
Short Tons :	1,295.561	913.958		2,209.519
Metric Tons in air :	1,175.315	829.130		2,004.445
Pounds in vacuo:	2,596,509.58	1,831,414.99		4,427,924.57
Metric Tons in vacuo :	1,177.758	830.717		2,008.475

For and on behalf of Oil Inspections USA Inc.: Ken Davis



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston

SUMMARY OF QUANTITIES

Page 2 of 2

Comparison of Ship's figures and Bill of Lading

US Barrels at 60°F :	LPG mix	Butane	Total
Bill of Lading	13,790.55	8,956.03	22,746.58
Vessel's loaded quantity	22,620.73		22,620.73
Difference			-125.85
% Difference			-0.553%
Bill of Lading	13,790.55	8,956.03	22,746.58
Vessel adjusted by VEF	22,618.47		22,618.47
Difference			-128.11
% Difference			-0.563%
US Gallons at 60°F :			Total
Bill of Lading	579,203.10	376,153.26	955,356.36
Vessel's loaded quantity	950,070.66		950,070.66
Difference			-5,285.70
% Difference			-0.553%
Bill of Lading	579,203.10	376,153.26	955,356.36
Vessel adjusted by VEF	949,975.66		949,975.66
Difference			-5,380.70
% Difference			-0.563%
Pounds in air :			Total
Bill of Lading	2,591,122.99	1,827,916.77	4,419,039.76
Vessel's loaded quantity	4,378,843.13		4,378,843.13
Difference			-40,196.63
% Difference			-0.910%
Bill of Lading	2,591,122.99	1,827,916.77	4,419,039.76
Vessel adjusted by VEF	4,378,405.29		4,378,405.29
Difference			-40,634.47
% Difference			-0.920%
Long Tons :			Total
Bill of Lading	1,156.751	816.034	1,972.785
Vessel's loaded quantity	1,954.841		1,954.841
Difference			-17.944
% Difference			-0.910%
Bill of Lading	1,156.751	816.034	1,972.785
Vessel adjusted by VEF	1,954.646		1,954.646
Difference			-18.139
% Difference			-0.919%
Metric Tons in air :			Total
Bill of Lading	1,175.315	829.130	2,004.445
Vessel's loaded quantity	1,986.212		1,986.212
Difference			-18.233
% Difference			-0.910%
Bill of Lading	1,175.315	829.130	2,004.445
Vessel adjusted by VEF	1,986.013		1,986.013
Difference			-18.432
% Difference			-0.920%
Metric Tons in vacuo :			Total
Bill of Lading	1,177.758	830.717	2,008.475
Vessel's loaded quantity	1,990.265		1,990.265
Difference			-18.210
% Difference			-0.907%
Bill of Lading	1,177.758	830.717	2,008.475
Vessel adjusted by VEF	1,990.066		1,990.066
Difference			-18.409
% Difference			-0.917%

For and on behalf of Oil Inspections USA Inc.: Ken Davis

CERTIFICATE OF QUANTITY LOADED

Report No.	US-0142-10-2014
Date of report	07-Oct-14
Vessel	Syn Mira
Location	ICT, Houston
Product	LPG mix, Butane
Bill of Lading date	07-Oct-14

Shore tank figures:

<u>GRAND TOTALS:</u>	<u>LPG mix</u>	<u>Butane</u>	<u>Grand Totals</u>
US Barrels at 60°F :	13,790.55	8,956.03	22,746.58
US Gallons at 60°F :	579,203.10	376,153.26	955,356.36
Pounds in air :	2,591,208.70	1,827,889.15	4,419,097.85
Long Tons :	1,156.788	816.022	1,972.810
Short Tons :	1,295.604	913.945	2,209.549
Metric Tons in air :	1,175.354	829.117	2,004.471
Metric Tons in vacuo :	1,177.812	830.703	2,008.515



RECEIPT FOR DOCUMENTS

Report No. US-0142-10-2014
Date of report 07-Oct-14
Vessel Syn Mira
Location ICT, Houston
Product LPG mix, Butane
Bill of Lading date 07-Oct-14

This is to confirm that I, undersigned Ship's Officer did receive from the undersigned Surveyor the following documents:

Document Title	Qty
Receipt For Documents	One
Time Log	One
Ullage Report before Loading (US units)	One
Ullage Report after Loading (US units)	One
Vessel Experience Report	One
Tank Inspection Report	One
Sample Receipt	One
Letter Of Protest on discrepancy for LPG mix	One
Letter Of Protest on discrepancy for Butane	One
Total Pages:	9

Instructions regarding documents:	1 set for Vessel's own use
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Should you have any query, or require any additional information, please contact Mr. Chris Sherfield at our Houston office (telephone number +1 281 488 7673).

Surveyor's name: Ken Davis

Chief Officer of "Syn Mira": Paul Garreth



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane
 Bill of Lading date 07-Oct-14

TIME LOG

Time	Date	Operations
11:30	30-Sep-14	Vessel arrived at roads (End of Sea Passage)
11:30	30-Sep-14	Notice of Readiness tendered
22:00	30-Sep-14	Vessel anchored - awaiting berthing instructions
08:00	06-Oct-14	Anchor aweigh - proceeding to berth
08:30	06-Oct-14	Pilot on board
09:42	06-Oct-14	Commenced mooring (first line ashore)
10:00	06-Oct-14	Vessel all fast alongside berth no. 4
12:30	06-Oct-14	Cleared by Customs / Free Pratique granted
12:36	06-Oct-14	Inspector on board
13:06	06-Oct-14	Tank inspection completed
13:06	06-Oct-14	OBQ calculation completed
13:36	06-Oct-14	Hoses connected (1 x 8" for liquid phase and 1 for vapor return line)
13:36	06-Oct-14	Commenced Loading
14:24	06-Oct-14	Notice of Readiness received/accepted
15:48	06-Oct-14	Completed Loading Butane
21:00	06-Oct-14	Commenced Loading LPG mix
08:42	07-Oct-14	Completed Loading (by ship)
09:48	07-Oct-14	Hose disconnected
10:06	07-Oct-14	Vessel's tanks measured
10:30	07-Oct-14	Loaded quantity calculation completed
11:30	07-Oct-14	Inspector's documents on board
11:45	07-Oct-14	Inspector left the vessel
12:15	07-Oct-14	Official cargo documents on board
16:54	07-Oct-14	Vessel sailed (ETS)

DELAYS				REASON
From		To		
11:30	30-Sep-14	08:30	06-Oct-14	Awaiting berthing instructions
08:30	06-Oct-14	10:00	06-Oct-14	Proceeding to the berth
12:36	06-Oct-14	13:36	06-Oct-14	Safety meeting
14:24	06-Oct-14	15:48	06-Oct-14	Awaiting permission from port authorities
20:30	06-Oct-14	21:00	06-Oct-14	Measurement / calculations
08:42	07-Oct-14	09:36	07-Oct-14	Cargo settlement
09:36	07-Oct-14	10:30	07-Oct-14	Measurement / calculations

Remarks: (*) - As per information received from the Master of the vessel

Sea water temperature, °F
58

General weather condition
calm

Product Name	Pumping time hours minutes	Bill of Lading Mt air	Pumping rate Mt air / hour
LPG mix	11 hours 42 minutes	1175.315	100.454
Butane	24 hours	829.130	34.547

Chief Officer of "Syn Mira":

Paul Garreth

Surveyor's name:

Ken Davis

VESSEL TANK INSPECTION REPORT

Report No. US-0142-10-2014
Date of report 07-Oct-14
Vessel Syn Mira
Location ICT, Houston
Product LPG mix, Butane
Bill of Lading date 07-Oct-14

Tank inspection was carried out: Time: 13:06 Date: 06-Oct-14

Inspection of "Syn Mira" at on October 6, 2014.

GENERAL INFORMATION

Name of Vessel: Syn Mira
Loading Place: ICT, Houston
Installation: LPG Terminal, berth No. 4
Date: 06-Oct-14
Cargoes to be loaded: LPG mix
Butane

INFORMATION OBTAINED ON BOARD

Previous cargoes: LPG mix in cargo tanks: 1P, 1S
LPG mix 2P, 2S
LPG mix 3P, 3S
Quantity remaining on board: 41.604 Metric Tons in air
Method of cleaning, if any: none

TEST RESULTS ON VAPOURS AFTER PURGING WITH NITROGEN

Oxygen Content, % by volume: Less than 0.3

CONCLUSION

As the oxygen content was below the limit of 0.3% by volume and previous cargo being compatible with cargoes to be loaded, all ships cargo tanks were found to be in a satisfactory condition to receive designated cargoes.

For receipt,
Chief Officer of "Syn Mira": Paul Garreth

For and on behalf of
Oil Inspections USA Inc.
Surveyor's name: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane
 Bill of Lading date 07-Oct-14

VESSEL ULLAGE REPORT BEFORE LOADING

Sea Condition : Calm
 Draft FWD : 9'4 3/16" TRIM : 7'4 9/16"
 AFT : 16'8 13/16" LIST : Nil

Tank No.	1P	1S	2P	2S	3P	3S		
Cargo	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix		
100% capacity of tanks:	3,323.03	3,318.57	4,681.13	4,692.51	4,688.93	4,695.53		

Liquid Phase

Observed Innage, Ft/In	0'	0'	0'	0'	0'	0'		
Correction for List, Ft/In								
Correction for Trim, Ft/In								
Corr'd Liquid Innage, Ft/In	0'	0'	0'	0'	0'	0'		
Liquid Volume, Barrels	0.00	0.00	0.00	0.00	0.00	0.00		
Liquid Temperature, °F	67.6	68.0	69.4	68.4	70.2	69.6		
Shrinking Factor	1.000000	1.000000	1.000000	1.000000	1.000000	1.000000		
Liquid Vol. corr'd, Barrels								
Rel. Density 60/60°F vacuo	0.5530	0.5530	0.5530	0.5530	0.5530	0.5530		
Density Lbs/Gall at 60°F air	4.6009	4.6009	4.6009	4.6009	4.6009	4.6009		
Liquid phase, V.C.F. by	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E		
Volume Correction Factor	0.99041	0.98990	0.98811	0.98939	0.98708	0.98785		
Net Liquid Volume, Barrels	0.00	0.00	0.00	0.00	0.00	0.00		

Vapour Phase

Vapor Volume, Barrels	3,323.03	3,318.57	4,681.13	4,692.51	4,688.93	4,695.53		
Inert gases, %								
Vol. Corr'd for In. Gas, bbls	3,323.03	3,318.57	4,681.13	4,692.51	4,688.93	4,695.53		
Vapor phase, V.C.F. by	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor		
Vapor Temperature, °F	67.6	68.0	69.4	68.4	70.2	69.6		
Shrinking Factor	1.000140	1.000150	1.000170	1.000160	1.000190	1.000180		
Volume corrected, Barrels	3,323.50	3,319.07	4,681.93	4,693.26	4,689.82	4,696.38		
Vapor Pressure, psi	53.81	53.81	52.79	52.79	54.82	54.82		
Vapor Cu Ft / Liquid Gall	32.783	32.783	32.783	32.783	32.783	32.783		
Vapor V.C.F.	0.0187346	0.0187204	0.0183928	0.0184277	0.0189175	0.0189389		
Net Liquid Volume, Barrels	62.26	62.13	86.11	86.49	88.72	88.94		
Subtotal, Barrels	62.26	62.13	86.11	86.49	88.72	88.94		

Before loading:

US Barrels at 60°F	62.26	62.13	86.11	86.49	88.72	88.94		
US Gallons at 60°F	2,614.92	2,609.46	3,616.62	3,632.58	3,726.24	3,735.48		
Pounds in air	12,030.99	12,005.86	16,639.71	16,713.14	17,144.06	17,186.57		
Long Tons	5.37	5.36	7.43	7.46	7.65	7.67		
Short Tons	6.02	6.00	8.32	8.36	8.57	8.59		
Metric Tons in air	5.46	5.45	7.55	7.58	7.78	7.80		

Total quantity before loading:

	<u>LPG mix</u>	<u>Total</u>
US Barrels at 60°F	474.65	474.65
US Gallons at 60°F	19,935.30	19,935.30
Pounds in air	91,720.33	91,720.33
Long Tons	40.947	40.947
Short Tons	45.860	45.860
Metric Tons in air	41.604	41.604
Metric Tons in vacuo	41.688	41.688

Remarks :

Vessel calculations based upon calibration tables

Chief Officer of "Syn Mira": Paul Garreth

For and on behalf of Oil Inspections USA Inc.: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane
 Bill of Lading date 07-Oct-14

VESSEL ULLAGE REPORT AFTER LOADING

Sea Condition : Calm
 Draft FWD : 19'0 3/8" TRIM : 0'7 7/8"
 AFT : 19'8 1/8" LIST : Nil

Tank No.	1P	1S	2P	2S	3P	3S		
Cargo	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix		
100% capacity of tanks:	3,323.03	3,318.57	4,681.13	4,692.51	4,688.93	4,695.53		

Liquid Phase

Observed Innage, Ft/In	23'1 3/16"	23'0 3/4"	23'5 1/8"	23'6 5/16"	25'0 13/16"	25'0 3/8"		
Correction for List, Ft/In								
Correction for Trim, Ft/In								
Corr'd Liquid Ullage, Ft/In	23'1 3/16"	23'0 3/4"	23'5 1/8"	23'6 5/16"	25'0 13/16"	25'0 3/8"		
Liquid Volume, Barrels	2,972.88	2,969.34	4,221.59	4,242.94	4,461.52	4,458.97		
Liquid Temperature, °F	66.2	66.6	74.2	77.8	67.3	64.9		
Shrinking Factor	1.000120	1.000126	1.000255	1.000325	1.000138	1.000099		
Liquid Vol. corr'd, Barrels	2,973.24	2,969.71	4,222.67	4,244.32	4,462.14	4,459.41		
Rel. Density 60/60°F vacuo	0.5539	0.5539	0.5539	0.5539	0.5539	0.5539		
Density Lbs/Gall at 60°F air	4.6088	4.6088	4.6088	4.6088	4.6088	4.6088		
Liquid phase, V.C.F. by	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E		
Volume Correction Factor	0.99222	0.99171	0.98201	0.97735	0.99083	0.99386		
Net Liquid Volume, Barrels	2,950.11	2,945.09	4,146.70	4,148.19	4,421.22	4,432.03		

Vapour Phase

Vapor Volume, Barrels	350.15	349.23	459.54	449.57	227.41	236.56		
Inert gases, %								
Vol. Corr'd for In. Gas, bbls	350.15	349.23	459.54	449.57	227.41	236.56		
VAPOR PHASE VCF by	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor	by Cu Ft Gas / Gal Liquid Factor		
Vapor Temperature, °F	68.4	68.7	77.2	77.2	67.3	65.5		
Shrinking Factor	1.000156	1.000162	1.000313	1.000313	1.000138	1.000108		
Volume corrected, Barrels	350.20	349.29	459.68	449.71	227.44	236.59		
Vapor Pressure, psi	79.77	79.77	78.32	78.32	78.32	78.32		
Vapor Cu Ft / Liquid Gall	33.132	33.132	33.132	33.132	33.132	33.132		
Vapor V.C.F.	0.0255231	0.0255086	0.0247193	0.0247193	0.0251838	0.0252701		
Net Liquid Volume, Barrels	8.94	8.91	11.36	11.12	5.73	5.98		
Subtotal, Barrels	2,959.05	2,954.00	4,158.06	4,159.31	4,426.95	4,438.01		

Loaded quantity:

US Barrels at 60°F	2,896.79	2,891.87	4,071.95	4,072.82	4,338.23	4,349.07		
US Gallons at 60°F	121,665.18	121,458.54	171,021.90	171,058.44	182,205.66	182,660.94		
Pounds in air	560,751.13	559,798.74	788,234.30	788,402.83	839,778.88	841,877.25		
Long Tons	250.34	249.91	351.89	351.97	374.90	375.84		
Short Tons	280.38	279.90	394.12	394.20	419.89	420.94		
Metric Tons in air	254.35	253.92	357.54	357.61	380.92	381.87		

Quantity loaded:

LPG mix

Butane

Total

US Barrels at 60°F	22,620.73		22,620.73
US Gallons at 60°F	950,070.66		950,070.66
Pounds in air	4,378,843.13		4,378,843.13
Long Tons	1,954.841		1,954.841
Short Tons	2,189.421		2,189.421
Metric Tons in air	1,986.212		1,986.212
Metric Tons in vacuo	1,990.265		1,990.265

Remarks :

Vessel calculations based upon calibration tables

Chief Officer of "Syn Mira": Paul Garreth

For and on behalf of Oil Inspections USA Inc.: Ken Davis

LETTER OF PROTEST ON APPARENT DISCREPANCY

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix, Butane
 Bill of Lading date 07-Oct-14

To: To Whom It May Concern

At the Port of:

Dear Sir,

On behalf of our principal(s), we hereby notify you that on the day of the following occurrence was noted:

APPARENT DISCREPANCY:

Total	LPG mix, Butane		
	US Gallons at 60°F :	US Barrels at 60°F :	Pounds in air :
Bill of Lading	955,356.36	22,746.58	4,419,039.76
Vessel's loaded quantity	950,070.66	22,620.73	4,378,843.13
Difference	-5,285.70	-125.85	-40,196.63
% Difference	-0.553%	-0.553%	-0.910%
Bill of Lading	955,356.36	22,746.58	4,419,039.76
Vessel adjusted by VEF	949,975.66	22,618.47	4,378,405.29
Difference	-5,380.70	-128.11	-40,634.47
% Difference	-0.563%	-0.563%	-0.920%
	Long Tons :	Metric Tons in air :	Metric Tons in vacuo :
Bill of Lading	1,972.785	2,004.445	2,008.475
Vessel's loaded quantity	1,954.841	1,986.212	1,990.265
Difference	-17.944	-18.233	-18.210
% Difference	-0.910%	-0.910%	-0.907%
Bill of Lading	1,972.785	2,004.445	2,008.475
Vessel adjusted by VEF	1,954.646	1,986.013	1,990.066
Difference	-18.139	-18.432	-18.409
% Difference	-0.919%	-0.920%	-0.917%

Accordingly, we are holding you responsible for the loss and damage thereby sustained, as well as any consequential arising therefrom.

Please direct any written correspondence on this matter to:

Mr. Chris Sherfield, Operations Manager
 Oil Inspections USA Inc.
 Tel. : +1 281 488 7673
 Cell : +1 713 253 2996
 Fax : +1 281 488 0495
 Email: chris_sherfield@oilinspections.com

Very truly yours:

Receipt acknowledged:

Date:
 Signed by:
 For: Surveyor

Date:
 Signed by:
 For:

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Bill of Lading date 07-Oct-14

SHORE TANK REPORT
Page 1 of 5
 Calculation in US Customary Units

		Tank No. 21		Tank No. 22		Tank No. 23	
LIQUID PHASE		Before	After	Before	After	Before	After
Product		LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix
Date	mm-dd-yy	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14
Time	0000						
Total Tank Volume	Barrels	3,863.55	3,863.55	3,788.98	3,788.98	3,835.50	3,835.50
Liquid level corrected, Feet & Inches		7'6 9/16"	1'2 3/4"	6'7 7/16"	1'2 7/8"	8'7 9/16"	1'5 5/16"
Liquid Volume	Barrels	1,720.20	113.32	1,414.74	116.20	2,042.43	147.28
Liquid Temperature	°F	71.8	65.7	70.0	62.1	70.3	69.6
Shrinkage Factor							
Liquid Volume Corrected	Barrels	1,720.20	113.32	1,414.74	116.20	2,042.43	147.28
Relative Density 60/60°F (in vacuo)		0.5356	0.5356	0.5346	0.5346	0.5345	0.5345
Density Lbs/Gall at 60°F in air		4.4561	4.4561	4.4478	4.4478	4.4470	4.4470
Density Lbs/Gall at 60°F in vac		4.4655	4.4655	4.4571	4.4571	4.4563	4.4563
Volume Correction Factor (CTL) determined by means of		ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E
Volume Correction Factor		0.98361	0.99215	0.98607	0.99711	0.98564	0.98663
Net Liquid Volume	Barrels	1,692.01	112.43	1,395.03	115.86	2,013.10	145.31
VAPOR PHASE							
Actual Vapor Volume	Barrels	2,143.35	3,750.23	2,374.24	3,672.78	1,793.07	3,688.22
Vapor Temperature	°F	67.3	55.6	73.4	56.5	73.0	61.5
Shrinkage Factor							
Vapor Vol. Corrected	Barrels	2,143.35	3,750.23	2,374.24	3,672.78	1,793.07	3,688.22
Vapor Pressure	psi	111.53	107.36	143.98	128.08	143.61	148.04
Cu feet of Vapor / Gall of Liquid		34.290	34.290	34.318	34.318	34.327	34.327
Vapor Volume Correction Factor		0.0330198	0.0326549	0.0410024	0.0381015	0.0409268	0.0429990
Net Liquid Volume	Barrels	70.77	122.46	97.35	139.94	73.38	158.59
Subtotal	Barrels	1,762.78	234.89	1,492.38	255.80	2,086.48	303.90
US Barrels at 60°F		1,762.78	234.89	1,492.38	255.80	2,086.48	303.90
US Gallons at 60°F		74,036.76	9,865.38	62,679.96	10,743.60	87,632.16	12,763.80
Pounds		329,915.21	43,961.12	278,787.93	47,785.38	389,700.22	56,760.62
Long Tons		147.284	19.626	124.459	21.333	173.973	25.340
Short Tons		164.958	21.981	139.394	23.893	194.850	28.380
Metric Tons in air		149.647	19.940	126.456	21.675	176.765	25.746
Metric Tons in vacuo		149.963	19.983	126.721	21.720	177.135	25.800
Difference, US Barrels at 60°F			1,527.89		1,236.58		1,782.58
Difference, US Gallons at 60°F			64,171.38		51,936.36		74,868.36
Difference, Pounds in air			285,954.09		231,002.55		332,939.60
Difference, Long Tons			127.658		103.126		148.633
Difference, Short Tons			142.977		115.501		166.470
Difference, Metric Tons in air			129.707		104.781		151.019
Difference, Metric Tons in vacuo			129.980		105.001		151.335
SUB TOTALS THIS PAGE:							
		Product :	LPG mix	Butane	Sub Totals		
US Barrels at 60°F :			4,547.05		4,547.05		
US Gallons at 60°F :			190,976.10		190,976.10		
Pounds in air :			849,896.24		849,896.24		
Long Tons :			379.417		379.417		
Short Tons :			424.948		424.948		
Metric Tons in air :			385.507		385.507		
Metric Tons in vacuo :			386.316		386.316		

For and on behalf of Oil Inspections USA Inc.: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Bill of Lading date 07-Oct-14

SHORE TANK REPORT
Page 2 of 5
 Calculation in US Customary Units

		Tank No. 24		Tank No. 25		Tank No. 26	
LIQUID PHASE		Before	After	Before	After	Before	After
Product		LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix
Date	mm-dd-yy	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14
Time	0000						
Total Tank Volume	Barrels	3,835.38	3,835.38	3,862.81	3,862.81	3,812.94	3,812.94
Liquid level corrected, Feet & Inches		8'5 1/8"	1'2 11/16"	12'5 1/8"	1'3 13/16"	6'8 1/8"	1'2 5/8"
Liquid Volume	Barrels	1,976.11	113.02	3,270.97	130.56	1,452.16	113.68
Liquid Temperature	°F	72.3	60.4	66.9	57.9	69.4	56.7
Shrinkage Factor							
Liquid Volume Corrected	Barrels	1,976.11	113.02	3,270.97	130.56	1,452.16	113.68
Relative Density 60/60°F (in vacuo)		0.5402	0.5402	0.5388	0.5388	0.5443	0.5443
Density Lbs/Gall at 60°F in air		4.4940	4.4940	4.4831	4.4831	4.5286	4.5286
Density Lbs/Gall at 60°F in vac		4.5034	4.5034	4.4924	4.4924	4.5380	4.5380
Volume Correction Factor (CTL) determined by means of		ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E
Volume Correction Factor		0.98333	0.99947	0.99064	1.00281	0.98758	1.00429
Net Liquid Volume	Barrels	1,943.17	112.96	3,240.35	130.93	1,434.12	114.17
VAPOR PHASE							
Actual Vapor Volume	Barrels	1,859.27	3,722.36	591.84	3,732.25	2,360.78	3,699.26
Vapor Temperature	°F	73.6	55.4	67.3	52.7	73.0	56.1
Shrinkage Factor							
Vapor Vol. Corrected	Barrels	1,859.27	3,722.36	591.84	3,732.25	2,360.78	3,699.26
Vapor Pressure	psi	154.86	112.45	141.94	103.35	146.26	111.00
Cu feet of Vapor / Gall of Liquid		33.980	33.980	34.054	34.054	33.716	33.716
Vapor Volume Correction Factor		0.0442332	0.0343409	0.0412592	0.0319807	0.0423649	0.0341684
Net Liquid Volume	Barrels	82.24	127.83	24.42	119.36	100.01	126.40
Subtotal	Barrels	2,025.41	240.79	3,264.77	250.29	1,534.13	240.57
US Barrels at 60°F		2,025.41	240.79	3,264.77	250.29	1,534.13	240.57
US Gallons at 60°F		85,067.22	10,113.18	137,120.34	10,512.18	64,433.46	10,103.94
Pounds		382,292.09	45,448.63	614,724.20	47,127.15	291,793.37	45,756.70
Long Tons		170.666	20.290	274.430	21.039	130.265	20.427
Short Tons		191.146	22.724	307.362	23.564	145.897	22.878
Metric Tons in air		173.405	20.615	278.835	21.377	132.355	20.755
Metric Tons in vacuo		173.768	20.658	279.413	21.421	132.630	20.798
Difference, US Barrels at 60°F			1,784.62		3,014.48		1,293.56
Difference, US Gallons at 60°F			74,954.04		126,608.16		54,329.52
Difference, Pounds in air			336,843.46		567,597.05		246,036.67
Difference, Long Tons			150.376		253.391		109.838
Difference, Short Tons			168.422		283.798		123.019
Difference, Metric Tons in air			152.790		257.458		111.600
Difference, Metric Tons in vacuo			153.110		257.992		111.832
SUB TOTALS THIS PAGE:		Product :	LPG mix	Butane	Sub Totals		
US Barrels at 60°F :			6,092.66		6,092.66		
US Gallons at 60°F :			255,891.72		255,891.72		
Pounds in air :			1,150,477.18		1,150,477.18		
Long Tons :			513.605		513.605		
Short Tons :			575.239		575.239		
Metric Tons in air :			521.848		521.848		
Metric Tons in vacuo :			522.934		522.934		

For and on behalf of Oil Inspections USA Inc.: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Bill of Lading date 07-Oct-14

SHORE TANK REPORT
Page 3 of 5
 Calculation in US Customary Units

LIQUID PHASE	Tank No. 30		Tank No. 31		Tank No. 37		
	Before	After	Before	After	Before	After	
Product	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	LPG mix	
Date	mm-dd-yy	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	
Time	0000						
Total Tank Volume	Barrels	3,870.16	3,870.16	3,896.35	3,896.35	3,812.36	3,812.36
Liquid level corrected, Feet & Inches		13'0 7/16"	4'1 15/16"	13'0 7/8"	10'3 5/16"	0'	0'
Liquid Volume	Barrels	3,302.97	748.88	3,291.42	2,527.13		
Liquid Temperature	°F	68.5	51.8	68.9	66.2	69.4	57.2
Shrinkage Factor							
Liquid Volume Corrected	Barrels	3,302.97	748.88	3,291.42	2,527.13		
Relative Density 60/60°F (in vacuo)		0.5368	0.5368	0.5360	0.5360	0.5360	0.5360
Density Lbs/Gall at 60°F in air		4.4662	4.4662	4.4593	4.4593	4.4593	4.4593
Density Lbs/Gall at 60°F in vac		4.4756	4.4756	4.4686	4.4686	4.4686	4.4686
Volume Correction Factor (CTL) determined by means of		ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E
Volume Correction Factor		0.98832	1.01102	0.98772	0.99147	0.98702	1.00381
Net Liquid Volume	Barrels	3,264.39	757.13	3,251.00	2,505.57	0.00	0.00
VAPOR PHASE							
Actual Vapor Volume	Barrels	567.19	3,121.28	604.93	1,369.22	3,812.36	3,812.36
Vapor Temperature	°F	69.6	55.0	69.8	57.0	69.4	57.0
Shrinkage Factor							
Vapor Vol. Corrected	Barrels	567.19	3,121.28	604.93	1,369.22	3,812.36	3,812.36
Vapor Pressure	psi	146.06	71.47	148.81	107.76	11.19	44.38
Cu feet of Vapor / Gall of Liquid		34.183	34.183	34.253	34.253	34.253	34.253
Vapor Volume Correction Factor		0.0420026	0.0231529	0.0426164	0.0327079	0.0067533	0.0157789
Net Liquid Volume	Barrels	23.82	72.27	25.78	44.78	25.75	60.15
Subtotal	Barrels	3,288.21	829.40	3,276.78	2,550.35	25.75	60.15
US Barrels at 60°F		3,288.21	829.40	3,276.78	2,550.35	25.75	60.15
US Gallons at 60°F		138,104.82	34,834.80	137,624.76	107,114.70	1,081.50	2,526.30
Pounds		616,803.75	155,579.18	613,710.09	477,656.58	4,822.73	11,265.53
Long Tons		275.359	69.455	273.978	213.240	2.153	5.029
Short Tons		308.402	77.790	306.855	238.828	2.411	5.633
Metric Tons in air		279.778	70.570	278.375	216.662	2.188	5.110
Metric Tons in vacuo		280.367	70.718	278.955	217.113	2.192	5.121
Difference, US Barrels at 60°F			2,458.81		726.43		-34.40
Difference, US Gallons at 60°F			103,270.02		30,510.06		-1,444.80
Difference, Pounds in air			461,224.57		136,053.51		-6,442.80
Difference, Long Tons			205.904		60.738		-2.876
Difference, Short Tons			230.612		68.027		-3.222
Difference, Metric Tons in air			209.208		61.713		-2.922
Difference, Metric Tons in vacuo			209.649		61.842		-2.929
SUB TOTALS THIS PAGE:							
	Product :	LPG mix	Butane				Sub Totals
US Barrels at 60°F :		3,150.84					3,150.84
US Gallons at 60°F :		132,335.28					132,335.28
Pounds in air :		590,835.28					590,835.28
Long Tons :		263.766					263.766
Short Tons :		295.417					295.417
Metric Tons in air :		267.999					267.999
Metric Tons in vacuo :		268.562					268.562

For and on behalf of Oil Inspections USA Inc.: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Bill of Lading date 07-Oct-14

SHORE TANK REPORT
Page 4 of 5
 Calculation in US Customary Units

		Tank No. 1		Tank No. 2		Tank No. 3	
LIQUID PHASE		Before	After	Before	After	Before	After
Product		Butane	Butane	Butane	Butane	Butane	Butane
Date	mm-dd-yy	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14
Time	0000						
Total Tank Volume	Barrels	3,730.52	3,730.52	3,747.73	3,747.73	3,766.75	3,766.75
Liquid level corrected, Feet & Inches		12'4 1/8"	1'1 9/16"	5'6 1/8"	1'0 11/16"	12'0 1/16"	2'10 11/16"
Liquid Volume	Barrels	3,141.68	106.54	1,151.88	98.88	3,070.62	459.11
Liquid Temperature	°F	68.4	65.5	69.4	67.1	65.1	67.1
Shrinkage Factor							
Liquid Volume Corrected	Barrels	3,141.68	106.54	1,151.88	98.88	3,070.62	459.11
Relative Density 60/60°F (in vacuo)		0.5841	0.5841	0.5839	0.5839	0.5842	0.5842
Density Lbs/Gall at 60°F in air		4.8602	4.8602	4.8589	4.8589	4.8609	4.8609
Density Lbs/Gall at 60°F in vac		4.8695	4.8695	4.8682	4.8682	4.8702	4.8702
Volume Correction Factor (CTL) determined by means of		ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E
Volume Correction Factor		0.99097	0.99410	0.98987	0.99237	0.99453	0.99238
Net Liquid Volume	Barrels	3,113.31	105.91	1,140.21	98.13	3,053.82	455.61
VAPOR PHASE							
Actual Vapor Volume	Barrels	588.84	3,623.98	2,595.85	3,648.85	696.13	3,307.64
Vapor Temperature	°F	78.8	67.8	87.4	71.2	86.5	70.0
Shrinkage Factor							
Vapor Vol. Corrected	Barrels	588.84	3,623.98	2,595.85	3,648.85	696.13	3,307.64
Vapor Pressure	psi	38.57	18.41	40.41	21.98	40.45	23.54
Cu feet of Vapor / Gall of Liquid		31.762	31.762	31.762	31.762	31.758	31.758
Vapor Volume Correction Factor		0.0147234	0.0093397	0.0149911	0.0102807	0.0150292	0.0107451
Net Liquid Volume	Barrels	8.67	33.85	38.91	37.51	10.46	35.54
Subtotal	Barrels	3,121.98	139.76	1,179.12	135.64	3,064.28	491.15
US Barrels at 60°F		3,121.98	139.76	1,179.12	135.64	3,064.28	491.15
US Gallons at 60°F		131,123.16	5,869.92	49,523.04	5,696.88	128,699.76	20,628.30
Pounds		637,284.78	28,528.99	240,627.50	27,680.57	625,596.66	100,272.10
Long Tons		284.502	12.736	107.423	12.357	279.284	44.764
Short Tons		318.642	14.264	120.314	13.840	312.798	50.136
Metric Tons in air		289.068	12.941	109.147	12.556	283.766	45.483
Metric Tons in vacuo		289.621	12.965	109.356	12.580	284.309	45.570
Difference, US Barrels at 60°F			2,982.22		1,043.48		2,573.13
Difference, US Gallons at 60°F			125,253.24		43,826.16		108,071.46
Difference, Pounds in air			608,755.79		212,946.93		525,324.56
Difference, Long Tons			271.766		95.066		234.520
Difference, Short Tons			304.378		106.474		262.662
Difference, Metric Tons in air			276.127		96.591		238.283
Difference, Metric Tons in vacuo			276.656		96.776		238.739
SUB TOTALS THIS PAGE:							
	Product :	LPG mix		Butane		Sub Totals	
US Barrels at 60°F :				6,598.83		6,598.83	
US Gallons at 60°F :				277,150.86		277,150.86	
Pounds in air :				1,347,027.28		1,347,027.28	
Long Tons :				601.352		601.352	
Short Tons :				673.514		673.514	
Metric Tons in air :				611.001		611.001	
Metric Tons in vacuo :				612.171		612.171	

For and on behalf of Oil Inspections USA Inc.: Ken Davis

Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Bill of Lading date 07-Oct-14

LIQUID PHASE	Tank No. 8		Tank No. 9		Tank No.	
	Before	After	Before	After	Before	After
Product	Butane	Butane	Butane	Butane		
Date	mm-dd-yy	07-Oct-14	07-Oct-14	07-Oct-14	07-Oct-14	
Time	0000					
Total Tank Volume	Barrels	3,760.78	3,760.78	3,731.59	3,731.59	
Liquid level corrected, Feet & Inches		6'4 1/8"	2'10 1/2"	9'3 15/16"	4'5 3/4"	
Liquid Volume	Barrels	1,386.63	438.48	2,294.99	849.85	
Liquid Temperature	°F	68.9	71.2	68.5	66.7	
Shrinkage Factor						
Liquid Volume Corrected	Barrels	1,386.63	438.48	2,294.99	849.85	
Relative Density 60/60°F (in vacuo)		0.5840	0.5840	0.5835	0.5835	
Density Lbs/Gall at 60°F in air		4.8593	4.8593	4.8556	4.8556	
Density Lbs/Gall at 60°F in vac		4.8686	4.8686	4.8649	4.8649	
Volume Correction Factor (CTL) determined by means of		ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E	ASTM Table 24E
Volume Correction Factor		0.99042	0.98792	0.99083	0.99278	
Net Liquid Volume	Barrels	1,373.35	433.18	2,273.94	843.71	
VAPOR PHASE						
Actual Vapor Volume	Barrels	2,374.15	3,322.30	1,436.60	2,881.74	
Vapor Temperature	°F	81.0	72.5	77.7	69.1	
Shrinkage Factor						
Vapor Vol. Corrected	Barrels	2,374.15	3,322.30	1,436.60	2,881.74	
Vapor Pressure	psi	40.79	26.34	22.10	17.34	
Cu feet of Vapor / Gall of Liquid		31.761	31.761	31.773	31.773	
Vapor Volume Correction Factor		0.0152748	0.0114772	0.0101883	0.0090133	
Net Liquid Volume	Barrels	36.26	38.13	14.64	25.97	
Subtotal	Barrels	1,409.61	471.31	2,288.58	869.68	
US Barrels at 60°F		1,409.61	471.31	2,288.58	869.68	
US Gallons at 60°F		59,203.62	19,795.02	96,120.36	36,526.56	
Pounds		287,688.15	96,189.94	466,722.02	177,358.36	
Long Tons		128.432	42.942	208.358	79.178	
Short Tons		143.844	48.095	233.361	88.679	
Metric Tons in air		130.493	43.631	211.702	80.448	
Metric Tons in vacuo		130.743	43.715	212.107	80.603	
Difference, US Barrels at 60°F			938.30		1,418.90	
Difference, US Gallons at 60°F			39,408.60		59,593.80	
Difference, Pounds in air			191,498.21		289,363.66	
Difference, Long Tons			85.490		129.180	
Difference, Short Tons			95.749		144.682	
Difference, Metric Tons in air			86.862		131.254	
Difference, Metric Tons in vacuo			87.028		131.504	
SUB TOTALS THIS PAGE:						
	Product :	LPG mix	Butane	Sub Totals		
US Barrels at 60°F :			2,357.20	2,357.20		
US Gallons at 60°F :			99,002.40	99,002.40		
Pounds in air :			480,861.87	480,861.87		
Long Tons :			214.670	214.670		
Short Tons :			240.431	240.431		
Metric Tons in air :			218.116	218.116		
Metric Tons in vacuo :			218.532	218.532		

For and on behalf of Oil Inspections USA Inc.: Ken Davis



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix
 Bill of Lading date 07-Oct-14
 Sample submitted as: LPG mix
 Sample drawn: by In-line autosampler
 Sample description: In-line autosample taken during loading
 Received on: 07-Oct-14
 Testing performed by: Third-party laboratory

ANALYSIS REPORT
(Grade 1: LPG mix)
During Loading

On the: 07-Oct-14

Test	Units	Method	Specification	Result
Composition liquid		ASTM D 2163 ASTM D 2421		
Methane	mass %			0.31%
Ethane	mass %			2.81%
Propane	mass %			46.84%
Propene (propylene)	mass %			0.02%
n-Butane	mass %			26.57%
Methyl propane (isobutane)	mass %			21.71%
trans-2-Butene	mass %			0.01%
cis-2-Butene	mass %			0.01%
n-Pentane	mass %			0.34%
2-Methyl butane (isopentane)	mass %			1.38%
Molecular Weight		Calculated		49.253
Relative Density 15.6/15.6°C (60/60°F) (in vacuo)		Calculated		0.5315
Density @ 15°C (in vacuo)	kg/l	Calculated		0.5318
Cu ft Gas / Gal Liquid		Calculated		34.1440
Density Lbs/Gall at 60°F (in vacuo)	Lbs/Gall	Calculated		4.4314
Density Lbs/Gall at 60°F (in air)	Lbs/Gall	Calculated		4.4221
Copper strip corrosion		ASTM D 1838		No. 1A
Hydrogen Sulphide	ppm	ASTM D 2420		Nil
Sulphur content	ppm	ASTM D 3246		4
Vapor pressure at 37.8 deg C	Kpa	ASTM D 1267		1412
Hydrogen Sulphide (H ₂ S)	%mass	ASTM 2420		Nil
Mercaptan Sulphur	ppm	UOP 212		Less 2
Free water content	ppm	ASTM D 1835		None
Volatile residue	volume %	ASTM D 1837		0.4
Residues in LPG by Gas Chromatography	ppm	ASTM D D7756		< 10 ppm
Methanol	ppm	ISO 8174		Nil

Chemist: Samantha Brown



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product Butane
 Bill of Lading date 07-Oct-14
 Sample submitted as: Butane
 Sample drawn: by In-line autosampler
 Sample description: In-line autosample taken during loading
 Received on: 07-Oct-14
 Testing performed by: Third-party laboratory

ANALYSIS REPORT
(Grade 2: Butane)
During Loading

On the: 07-Oct-14

Test	Units	Method	Specification	Result
Composition liquid		ASTM D 2163 ASTM D 2421		
Ethane	mass %			0.01%
Propane	mass %			0.16%
n-Butane	mass %			97.89%
Methyl propane (isobutane)	mass %			0.88%
1-Butene	mass %			0.07%
trans-2-Butene	mass %			0.08%
cis-2-Butene	mass %			0.04%
2-Methyl propene (isobutylene)	mass %			0.04%
1,3-Butadiene	mass %			0.01%
n-Pentane	mass %			0.03%
2-Methyl butane (isopentane)	mass %			0.79%
Molecular Weight		Calculated		58.175
Relative Density 15.6/15.6°C (60/60°F) (in vacuo)		Calculated		0.5842
Density @ 15°C (in vacuo)	kg/l	Calculated		0.5842
Cu ft Gas / Gal Liquid		Calculated		31.7690
Density Lbs/Gall at 60°F (in vacuo)	Lbs/Gall	Calculated		4.8706
Density Lbs/Gall at 60°F (in air)	Lbs/Gall	Calculated		4.8613
Copper strip corrosion		ASTM D 1838		No. 1A
Hydrogen Sulphide	ppm	ASTM D 2420		Nil
Sulphur content	ppm	ASTM D 3246		4
Vapor pressure at 37.8 deg C	Mpa	ASTM D 1267		283
Hydrogen Sulphide (H ₂ S)	ppm	UOP 212		Nil
Carbonyl Sulphide (COS)	ppm	UOP 212		2.5
Free water content	ppm	ASTM D 1835		None
Volatile residue	volume %	ASTM D 1837		0.8
Residues in LPG by Gas Chromatography	ppm	ASTM D D7756		< 10 ppm
Methanol	ppm	ISO 8174		Nil

Chemist:



Report No. US-0142-10-2014
 Date of report 07-Oct-14
 Vessel Syn Mira
 Location ICT, Houston
 Product LPG mix
 Bill of Lading date 07-Oct-14
 Sample submitted as: LPG mix
 Sample drawn: by Oil Inspections USA Inc. surveyor
 Sample description: Multiple-ship's tank composite taken after loading
 Received on: 07-Oct-14
 Testing performed by: Third-party laboratory

ANALYSIS REPORT
(Grade 1: LPG mix)
After Loading

On the: 07-Oct-14

Test	Units	Method	Specification	Result
Composition liquid		ASTM D 2163 ASTM D 2421		
Methane	mass %			0.17%
Ethane	mass %			1.55%
Propane	mass %			25.92%
Propene (propylene)	mass %			0.01%
n-Butane	mass %			58.52%
Methyl propane (isobutane)	mass %			12.38%
1-Butene	mass %			0.03%
trans-2-Butene	mass %			0.04%
cis-2-Butene	mass %			0.02%
2-Methyl propene (isobutylene)	mass %			0.02%
n-Pentane	mass %			0.21%
2-Methyl butane (isopentane)	mass %			1.13%
Molecular Weight		Calculated		52.894
Relative Density 15.6/15.6°C (60/60°F) (in vacuo)		Calculated		0.5539
Density @ 15°C (in vacuo)	kg/l	Calculated		0.5541
Cu ft Gas / Gal Liquid		Calculated		33.1330
Density Lbs/Gall at 60°F (in vacuo)	Lbs/Gall	Calculated		4.6183
Density Lbs/Gall at 60°F (in air)	Lbs/Gall	Calculated		4.6089
Copper strip corrosion		ASTM D 1838		No. 1A
Hydrogen Sulphide	ppm	ASTM D 2420		Nil
Sulphur content	ppm	ASTM D 3246		4
Vapor pressure at 37.8 deg C	KPa	ASTM D 1267		808
Hydrogen Sulphide (H2S)	ppm	UOP 212		Nil
Mercaptan Sulphur	ppm	UOP 212		2
Free water content	ppm	ASTM D 1835		None
Volatile residue	volume %	ASTM D 1837		0.57
Residues in LPG by Gas Chromatography	ppm	ASTM D D7756		< 10 ppm
Methanol	ppm	ISO 8174		Nil

Chemist: